



Original article

Molecular dynamics simulations of oil recovery from dolomite slit nanopores enhanced by CO₂ and N₂ injection

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Keywords:

Molecular dynamics simulations
CO₂ and N₂ flooding
shale oil
interaction energy

Cited as:

Guo, H., Wang, Z., Wang, B., Zhang, Y., Meng, H., Sui, H. Molecular dynamics simulations of oil recovery from dolomite slit nanopores enhanced by CO₂ and N₂ injection. *Advances in Geo-Energy Research*, 2022, 6(4): 306-313.
<https://doi.org/10.46690/ager.2022.04.05>

Abstract:

Shale oil reservoirs are dominated by micro- and nanopores, which greatly impede the oil recovery rates. CO₂ and N₂ injection have proven to be highly effective approaches to enhance oil recovery from low-permeability shale reservoirs, and also represent great potential for CO₂ sequestration. Therefore, a better understanding of the mechanism of shale oil recovery enhanced by CO₂ and N₂ is of great importance to achieve maximum shale oil productivity. In this paper, the adsorption behavior of shale oil and the mechanism of enhancing shale oil recovery by CO₂ and N₂ flooding in dolomite slit pores are investigated by performing nonequilibrium molecular dynamics simulations. Considering the shale oil adsorption behavior, mass density distribution is analyzed and the results indicate that a symmetric density distribution of the oil regarding the center in the slit pore along the *x*-axis can be obtained. The maximum density of the adsorbed layer nearest to the slit wall is 1.310 g/cm³ for C₈H₁₈, which is about 2.0 times of that for bulk oil density in the middle area of slit pore. The interaction energy and radial distribution functions (between oil and CO₂, and between oil and N₂) are calculated to display the displacement behavior of CO₂ and N₂ flooding. It is found that CO₂ and N₂ play different roles: CO₂ has strong solubility, diffusivity and a higher interaction energy with dolomite wall, and the oil displacement efficiency of CO₂ reaches 100% after 1 ns of flooding; however, during N₂ flooding, the oil displacement efficiency is 87.3% after 4 ns of flooding due to the lower interaction energy between N₂ and dolomite and that between N₂ and oil.

1. Introduction

With the development of modern industrial technology, such as horizontal drilling and hydraulic fracturing, the exploitation of shale oil can influence the global energy supply and subsequently mitigate the worldwide energy crisis and environmental issues, which has led to a “shale revolution” (Hughes, 2013; Zeng et al., 2020; Cai et al., 2022). Many scholars have studied the properties of oil in shale by performing empirical calculations (Panja et al., 2019; Wu et al., 2019; Zhao et al., 2020) and macroscopic simulation experiments (Tovar et al., 2020). The adsorption behavior and transport mechanism were reported as highly complex

and difficult to understand due to the pervasive presence of nanopore throat networks and the extremely small permeability of the shale matrix (de Almeida and Miranda, 2016; Yang et al., 2020). Omnipresent nanopores and low permeability present significant challenges during oil exploitation processes for shale (Wu et al., 2020).

In recent years, both theoretical and experimental methods as well as some field tests (Seyyedsar and Sohrabi, 2017; Singh, 2018) were broadly applied for extracting crude oil by CO₂ injection. Han et al. (2016) studied the effects of gravity segregation on both oil production and CO₂ sequestration by a 2D CO₂ flooding apparatus in vertical and horizontal

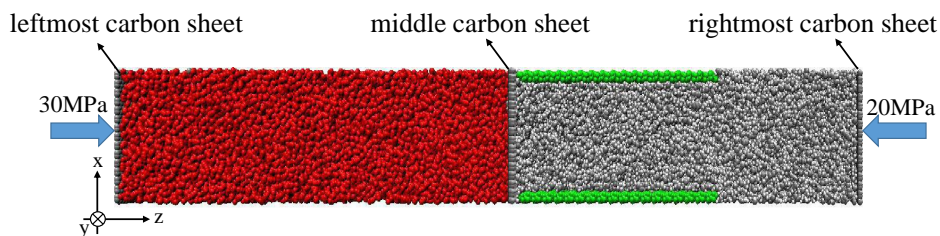


Fig. 1. Snapshot of the initial system configurations (red, CO₂ molecules; green, dolomite pore; gray, C₈H₁₈ molecules).

sandstone systems, and the results indicated that the CO₂ has better storage efficiency in a miscible system. Zhou et al. (2019) conducted three types of CO₂ injection experiments to study oil production in a tight oil reservoir. The results revealed that the best method for enhanced oil recovery (EOR) was the injection of CO₂ in tight formations, and the crude oil recovery was indicated to reach 38.96%.

Despite the above advancements, some obvious disadvantages of CO₂ enhanced oil recovery have emerged, for example, higher production costs. Compared with CO₂, N₂ has the advantages of low cost, no corrosion, sufficient supply and ease of maintaining formation pressure (Potoff and Siepmann, 2001). It is widely known that the minimum miscibility pressure of gas-oil is a key parameter to evaluate the cost and feasibility of miscible flooding of gas EOR. Miscible N₂ flooding is a relatively rarely applied EOR technology in most oil reservoirs due to the requirement of high pressure to reach miscibility (Mogensen and Xu, 2020), which may lead to unexpectedly low replacement efficiency (Siregar et al., 2007). Mogensen and Xu (2020) found that miscible N₂ injection was a viable option to increase oil recovery. The density and viscosity of reservoir fluid could be increased by N₂ injection and the oil recovery was 10%-20% higher than that for water flood.

A direct and convenient approach to study the properties of oil in shale is to perform experiments (Anovitz and Cole, 2015; Gu et al., 2015; Haagh et al., 2018); however, the effect of surface anisotropy and high-pressure conditions, like those of the formation pressure in shale, cannot be easily predicted in this way. Scanning electron microscopy can clearly visualize the nanopores (Curtis et al., 2010; Eberle et al., 2016), but the pore structure or surface of rock samples possibly get damaged in the process. Although lab studies can well demonstrate the oil displacement efficiency by the injection of CO₂ or N₂, they cannot be used to explain the complex interactions, such as the changes in viscosity, density, specific volume, and swelling of crude oil after CO₂ or N₂ injection, or the oil displacement mechanism at the molecular level.

In the past few years, molecular dynamics by simulation has proved as a useful tool for studying the dynamical, structural properties in microscopic scale, and reveal the spatial distribution and trajectory of gas and oil molecules (Sui and Yao, 2016; Mohammed and Gadikota, 2019; Aminian and ZareNezhad, 2021). Mejía et al. (2014) combined experiments and molecular simulations to investigate the mixing processes of CO₂-oil molecules on tension measurements, coexisting densities, density profiles, and relative Gibbs adsorption

isotherms regarding the interfacial region. Fang et al. (2021) performed molecular simulations to study the behavior of gas injection and reveal the interaction between gas and oil at different reservoir depths. Zhang et al. (2021) found that CO₂ was preferably adsorbed on the calcite wall surface, forming a thin CO₂ film based on strong the interaction between oil and CO₂ molecules.

In this work, to address the issues mentioned above, the behaviors during the oil displacement process of CO₂ and N₂ injection and adsorption were studied by molecular simulations. First, the adsorption behavior was analyzed to reveal the oil distribution characteristics. Then, by scrutinizing the microscopic interaction, adsorption characteristics, and interface effect during the flooding process, the mechanism of migration behavior for shale oil was revealed. Dolomite, which has attracted many scholars' attention in subject areas (Tutolo et al., 2014; Berninger et al., 2017), was selected as reservoir matrix due to it being a common rock-forming mineral in carbonate reservoirs.

2. Methodology

2.1 Molecular models

Dolomite is the main component of shale in the Permian Lucaogou Formation of the Jimusar sag, which was selected as a typical mineral component. A repeat unit of dolomite was cleaved along the crystallographic orientation (1 -1 0) (Sui et al., 2020), and then a dolomite model supercell was rebuilt with dimensions of $x = 65.45 \text{ \AA}$, $y = 38.51 \text{ \AA}$ and $z = 138.83 \text{ \AA}$ to meet the slit pore width of 57 \AA .

Saturated linear alkanes-octane (C₈H₁₈) was used to represent shale oil in the present work (Wang et al., 2015). The oil molecules were placed in the dolomite pore. All oil molecules were considered fully flexible, and a 4 ns equilibrium molecular dynamics simulation with a timestep of 1 fs on the simulation box with the canonical ensemble was performed to reduce the energy state and obtain a reasonable oil density. The gas (CO₂ or N₂) box was positioned on the left side of the dolomite slit pore to generate a pressure differential along the z -axis. The simulation model is shown in Fig. 1.

2.2 Simulation methods

The Large-scale Atomic/Molecular Massively Parallel Simulator package (Plimpton, 1995) was used to perform all of the molecular dynamics simulations. The interactions between atoms were described by the COMPASS (condensed-phase optimized molecular potential for atomistic simulation studies)

class II force field (Sun, 1998; Sun et al., 2016). This force field is expressed by:

$$E = E_{val} + E_{cro} + E_{non} \quad (1)$$

$$E_{val} = \sum_b [A_2(b - b_0)^2 + A_3(b - b_0)^3 + A_4(b - b_0)^4] \\ + \sum_\phi [B_2(\phi - \phi_0)^2 + B_3(\phi - \phi_0)^3 + B_4(\phi - \phi_0)^4] \\ + \sum_\gamma [C_1(1 - \cos \gamma) + C_2(1 - \cos 2\gamma) + C_3(1 - \cos 3\gamma)] \\ + \sum_\chi D\chi^2 \quad (2)$$

$$E_{cro} = \sum_{b,b'} H_{bb'}(b - b_0)(b - b'_0) + \sum_{b,\phi} H_{b\phi}(b - b_0)(\phi - \phi_0) \\ + \sum_{b,\gamma} (b - b_0)(H_1 \cos \gamma + H_2 \cos 2\gamma + H_3 \cos 3\gamma) \\ + \sum_{\phi,\gamma} (\phi - \phi_0)(F_1 \cos \gamma + F_2 \cos 2\gamma + F_3 \cos 3\gamma) \\ + \sum_{b,\phi} V(\phi - \phi_0)(\phi - \phi'_0) + \sum_{b,\phi,\gamma} Y(\phi - \phi_0)(\phi - \phi'_0) \quad (3)$$

$$E_{non} = E_{vdW} + E_{ele} \\ = \sum \epsilon_{LJ} \left[2 \left(\frac{r_{ij}^0}{r_{ij}} \right)^9 - 3 \left(\frac{r_{ij}^0}{r_{ij}} \right)^6 \right] + \sum \frac{q_i q_j}{r_{ij}} \quad (4)$$

The E_{val} , E_{cro} , E_{non} , E_{vdW} and E_{ele} represent valence energy, cross-term interaction energy, non-bonding interaction term, van der Waals interaction energy and electrostatic interaction energy, respectively. In Eqs. (1)-(4), q_i and q_j denote the charge of the i -th and j -th atoms, ϵ_{LJ} denotes the dielectric constant, and r_{ij} is the distance between atom i and atom j atomic. The parameters b , ϕ , γ and χ are bond length, bond angle, dihedral torsion angle and out of plane angle. b_0 , b'_0 , ϕ_0 , ϕ'_0 , A_i ($i = 1 - 4$), B_i ($i = 2 - 4$), C_i ($i = 1 - 3$), D , H_{bb} , $H_{b\phi}$, H_i ($i = 1 - 3$), F_i ($i = 1 - 3$), V and Y are fitted by quantum mechanical calculations. The parameters for dolomite, CO₂ and C₈H₁₈ are listed in Table 1.

For this simulation step, firstly, the oil molecules were placed on the right side of the pore, and a carbon sheet (middle) was put on the left side of the dolomite pore to make

it rigid and fixed. The fixed carbon sheet also kept oil away from CO₂ molecules before the flooding simulation, and 20 MPa pressure was applied to the rightmost carbon sheet along the z -axis to push the oil molecules into the pores. During the flooding simulation, the middle carbon sheet was removed, and 30 MPa pressure was applied to the leftmost carbon sheet along the z -axis to ensure the pressure difference of 10 MPa between the two sheets. Then, the CO₂ molecules were pushed into the pores to drive the oil phase across the channel.

All molecular dynamics simulations were performed by a canonical ensemble using the Velocity Verlet algorithm (Yoshida, 1990). The integration step was set as 1.0 fs, and 15.0 ns of simulation was conducted. Next, the trajectories were collected and used for data analysis, followed by the discussion of the properties of oil or gas in dolomite slit nanopores. The Nose-Hoover method (Martyna et al., 1994) was employed to control the temperature of the system, which was kept at 333 K. The van der Waals (vdW) interactions were calculated within a cutoff distance of 10.5 Å, and the particle-particle-mesh (pppm) summation method (Hockney et al., 1974) with a relative error of 1×10^{-5} used to calculate the long-range interactions. Periodic boundary conditions were applied in all three dimensions. The configuration snapshots were rendered by visual molecular dynamics software (Fernandes et al., 2019).

3. Results and discussion

3.1 Density distribution

Prior to gas injection development, the mass density profiles of oil phase in the dolomite slit pores were calculated. The oil phase density could be computed based on the molecular centroid. Here, the slit pores were first divided into some slabs along the x direction, with each slab at 0.5 Å, and then the mass density could be determined in each slab (Wang et al., 2021). Fig. 2 shows the alkane density distributions in the dolomite slit pore. Obviously, a symmetric density distribution of C₈H₁₈ regarding the pore center can be obtained. The oscillations of density distribution indicate that oil molecules form 4 similar layered adsorption structures near the two opposing walls. The result shows that oil molecules are subjected to large forces from the wall confined in nanoscale mineral pores, such as vdW and electrostatic interactions. Due to the high energy barrier between the adsorption layers, the dense adsorbed layer will limit the movement of oil molecules. The width of each adsorption layer between two adjacent density peaks (or valleys) was 5.0 Å, which is consistent with the measurement of solvation force (Christenson et al., 1987), and similar to those from previous studies (Wang et al., 2016; Sui et al., 2020). The first adsorption layer mass density was 1.322 g/cm³ for C₈H₁₈, which is about 2.0 times greater than that for bulk oil phase density in the pore center. In the pore center, the density of C₈H₁₈ was 0.661 g/cm³, in good agreement with the result (0.659 g/cm³) predicted by the National Institute of Standards and Technology Chemistry WebBook, which enhanced the correctness of our simulation and validates the simulation method.

Table 1. LJ-9-6 function parameters for dolomite, CO₂ and C₈H₁₈.

	ϵ (kcal/mol)	r^0 (Å)
O (dolomite)	0.067	3.360
Ca (dolomite)	0.112	3.400
Mg (dolomite)	0.046	2.600
C (dolomite)	0.070	3.900
C (CO ₂)	0.068	3.915
O (CO ₂)	0.067	3.360
C (C ₈ H ₁₈)	0.062	3.854
H (C ₈ H ₁₈)	0.023	2.878

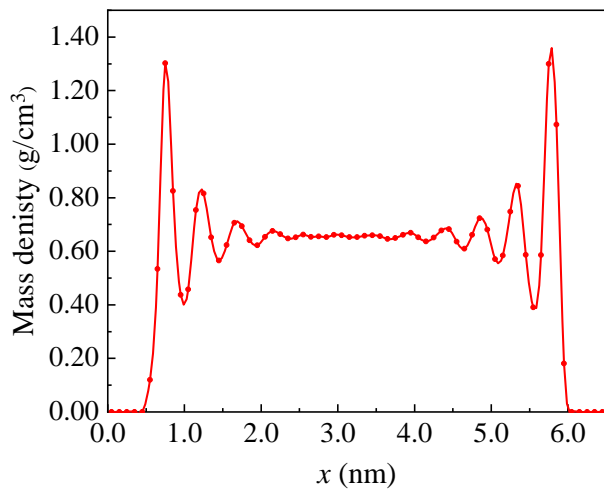


Fig. 2. Mass density for C_8H_{18} in dolomite slit pore before gas flooding (20 MPa, 333 K).

3.2 Displacement behavior of CO_2 and N_2

A number of snapshots of the CO_2 injection process, the density variation of C_8H_{18} and CO_2 along the z -axis, and the number of C_8H_{18} and CO_2 at different times in dolomite slit pores are shown in Fig. 3. At $t = 0$ ns, there is an obvious interface between oil and gas, and oil molecules stay and are absorbed on the dolomite surface. With the time passing, the CO_2 molecules are injected into the dolomite pore, and they will occupy the position of oil molecules and replace them. CO_2 will also replace oil molecules adsorbed on the wall and create a film between them and the wall, as seen in Fig. 3(d), which is important for the separation of oil molecules from the dolomite surface and is beneficial to oil recovery. After 0.5 ns of flooding, the density profiles along the z -axis within the slit pore were computed to present a detailed density profile of the CO_2 and oil mixtures in Fig. 3(b), which showed that the density difference at the flooding frontier was gradual, and

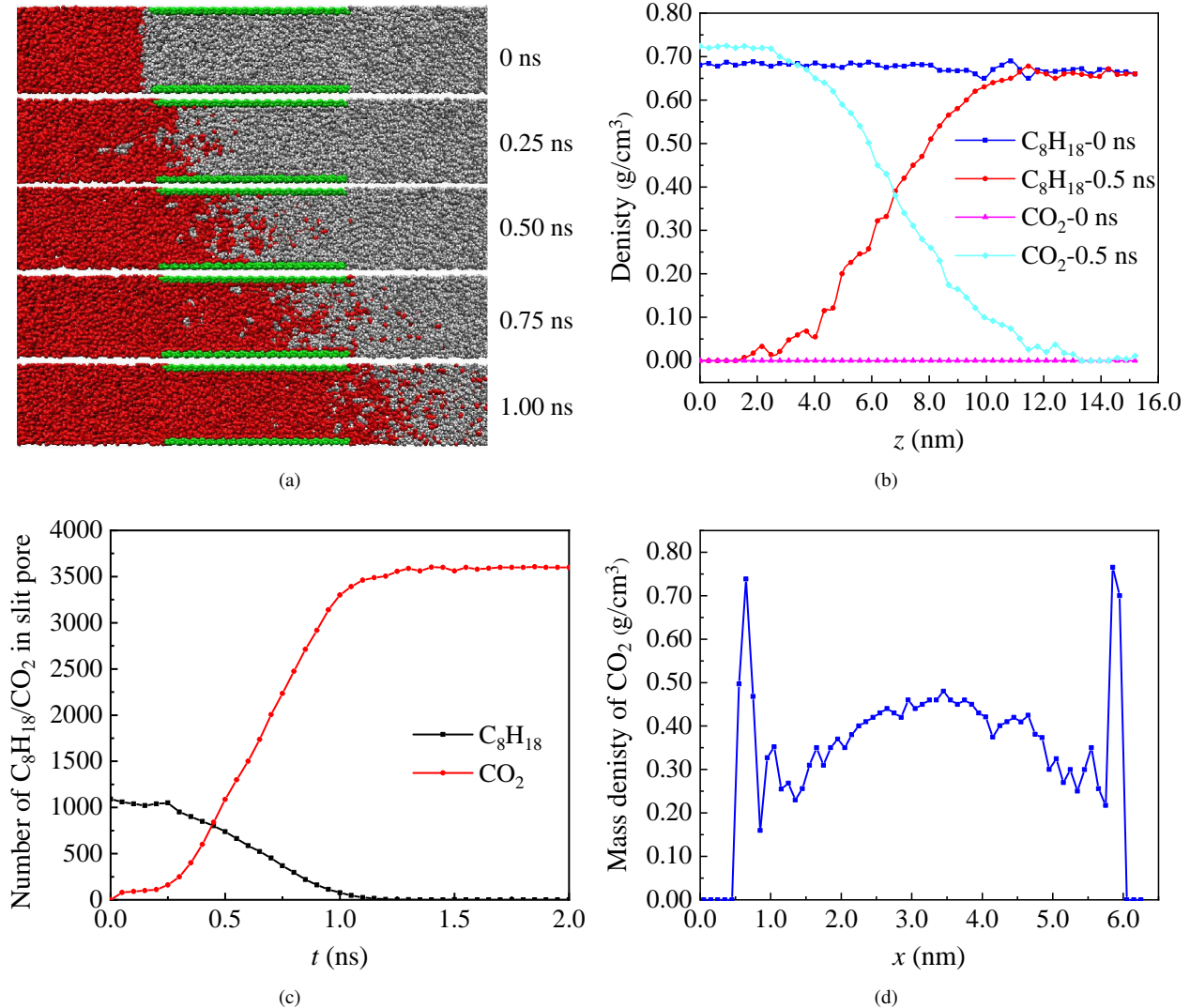


Fig. 3. (a) Snapshots to indicate the evolutions of CO_2 flooding (red: CO_2 molecule, gray: oil phase, green: dolomite); (b) Density profiles along the z -axis within the slit pore; (c) Amount of CO_2 and residual oil molecules in nanoslit during CO_2 flooding; (d) Density profiles of CO_2 along the x -axis within the slit pore after 0.5 ns of flooding.

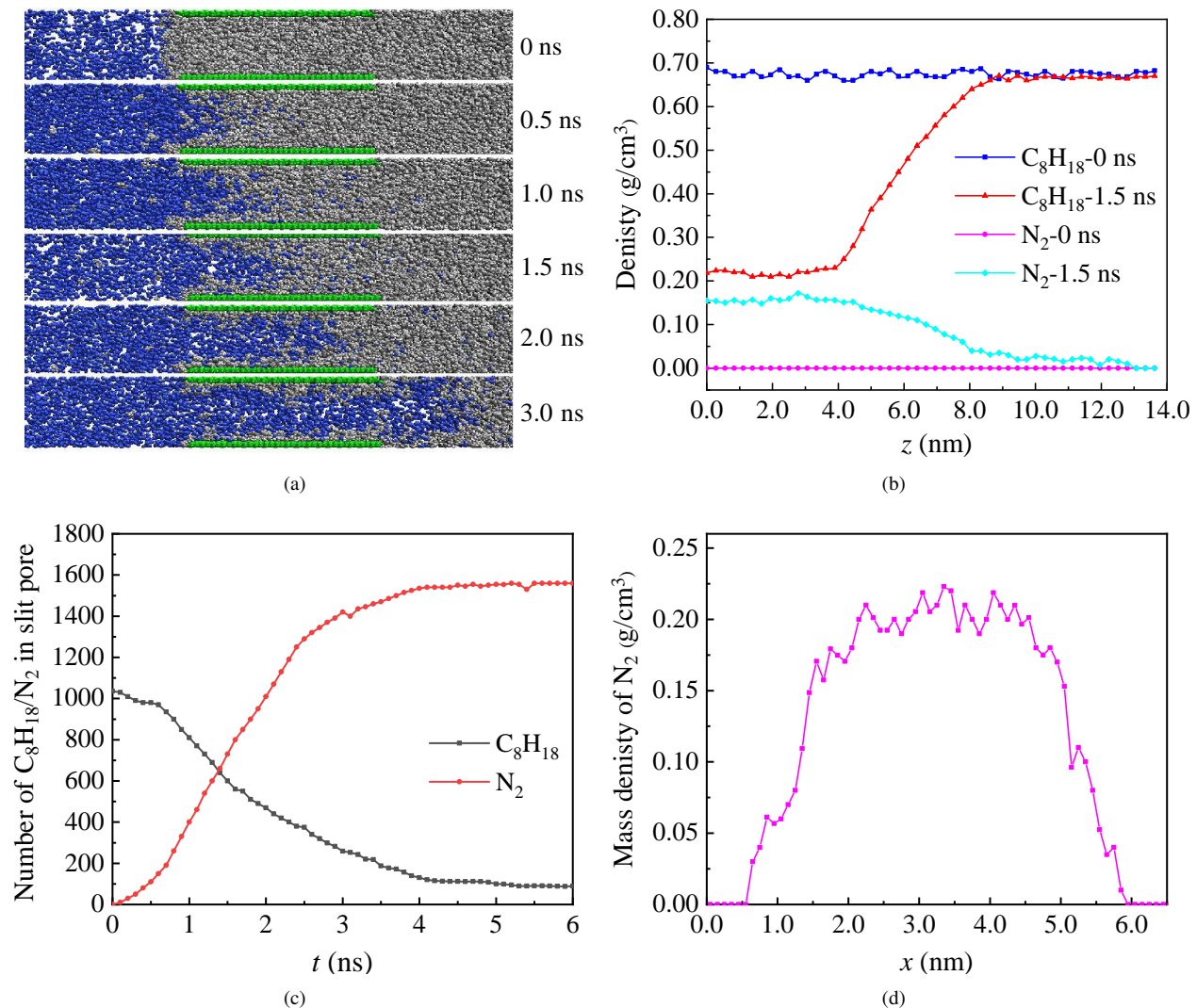


Fig. 4. (a) Snapshots depicting the evolutions of N₂ flooding (blue: N₂ molecule, gray: oil phase, green: dolomite); (b) Density profiles along the *z*-axis within the slit pore; (c) Number of N₂ and residual oil molecules in nanoslits during N₂ flooding; (d) Density profiles of N₂ along the *x*-axis within the slit pore after 2.0 ns of flooding.

there was actually no obvious interface between CO₂ and oil. In other words, almost all CO₂ molecules were dissolved in the oil phase at the gas-oil interface, indicating the good solution and diffusion properties of CO₂ molecules. Fig. 3(c) shows the amount of CO₂ and oil molecules in slit pores after CO₂ flooding. It is seen that after 1.0 ns of CO₂ flooding, almost all oil molecules have been driven out of the slit pores.

Fig. 4. shows the N₂ injection snapshots, the density of C₈H₁₈ and N₂ along the *z*-axis, and the number of C₈H₁₈ and N₂ at different time points in the dolomite slits. There is also an obvious interface between the oil and N₂ molecules; oil molecules remain and are absorbed on the dolomite surface at 0 ns. The snapshots in Fig. 4(a) indicate that there is an interface between N₂ and oil from the flooding frontier at different time points. Fig. 4(b) shows the density curve of oil and N₂ along the *z*-axis after 1.5 ns of flooding. From the figure, we can find that the density variation interval from 4 to 8 nm within the dolomite slit pore is shorter than that

during CO₂ flooding (after 0.5 ns of flooding, from 2 to 10 nm, see Fig. 3(b)), which means that the N₂ molecules have poor dissolution and diffusion properties compared to CO₂ in C₈H₁₈ molecules. Fig. 4(c) depicts the number of oil and N₂ molecules remaining in the slit pores of N₂ flooding. It can be found that some oil molecules remain near the pore walls after 4 ns of N₂ flooding. Fig. 4(d) illustrates the density profiles of N₂ along the *x*-axis within the slit pore after 2.0 ns of flooding. Clearly, the N₂ density is low near the wall surface, indicating that oil molecules at the wall have not been displaced, that is, as for the N₂ injection, the N₂ molecules form a dominant path and pass through the oil phase in the slit pores.

The variation of oil molecule number during CO₂ and N₂ flooding within dolomite slit pores was studied and presented above in Figs. 3 and 4. These results show that the CO₂ molecules have better dissolution and diffusion properties than the N₂ molecules. During CO₂ flooding, almost all oil molecules will be driven out, but there will be some oil

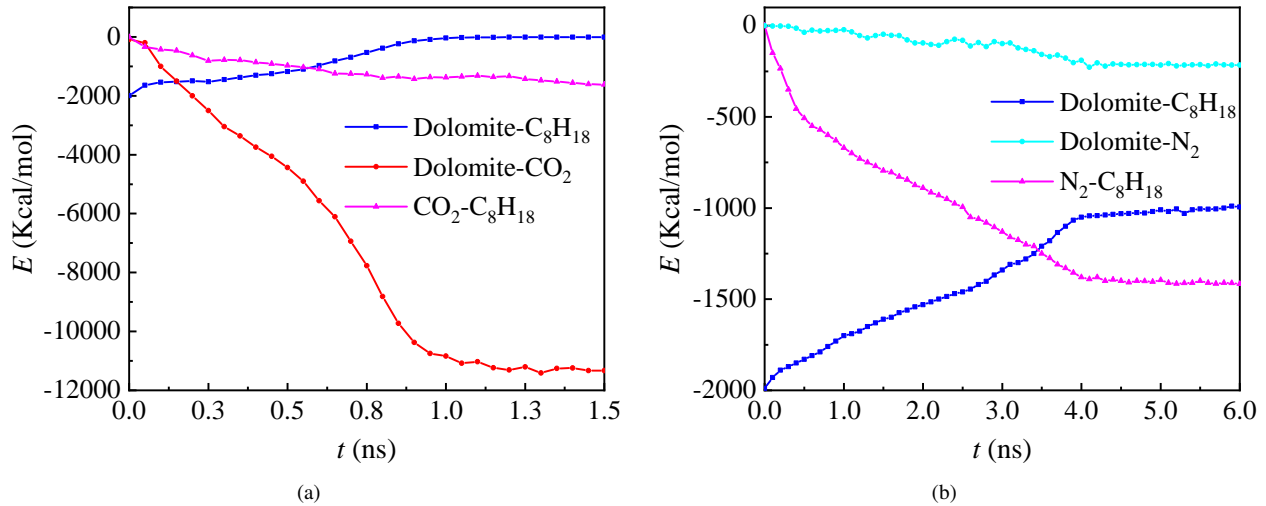


Fig. 5. Interaction energy profiles between oil molecules and dolomite wall under (a) CO₂ injection, and (b) N₂ injection.

molecules staying within the slit pores after the N₂ injections.

In order to clarify the nature of flooding behaviour, i.e., the dissolution and retention of octane during CO₂ and N₂ flooding, the interactions between gas phase, dolomite wall and the oil molecules were studied as shown in Fig. 5. The interaction energy can be computed by Eq. (5) (Li et al., 2016). Here, the interaction energy between octane and gas is displayed as follows:

$$E_{int} = E_{total} - (E_{gas} - E_{oct}) \quad (5)$$

where E_{int} represents the interaction energy between gas and octane, E_{total} represents the total energy, and E_{gas} and E_{oct} denote the gas and the octane energy, respectively.

Fig. 5(a) shows the interaction energy of dolomite-CO₂, dolomite-C₈H₁₈ and C₈H₁₈-CO₂ during CO₂ flooding. We can find that the interaction energy between dolomite wall and CO₂ increases gradually with time until 1 ns of CO₂ flooding. On the contrary, the interaction energy between dolomite wall and C₈H₁₈ decreases gradually with time up to 1 ns when CO₂ molecules have filled the pores and all oil molecules have been driven out. The interaction energy between dolomite wall and CO₂ is greater than that between the dolomite wall and C₈H₁₈ molecules, hence CO₂ can occupy the dolomite surface and expel oil molecules from the dolomite surface. In addition, the high attraction between C₈H₁₈ and CO₂ can cause the CO₂ molecules to disperse into the C₈H₁₈ phase, which can enhance the C₈H₁₈ mobility due to its reduced viscosity.

Fig. 5(b) demonstrates the interaction energy of dolomite-N₂, dolomite-C₈H₁₈ and C₈H₁₈-N₂. During N₂ flooding, the interaction energy between dolomite and N₂ is always smaller than that between dolomite and C₈H₁₈ molecules during the whole flooding process from 0 to 6 ns. Thus, the N₂ molecules cannot peel off the oil molecules adsorbed on the dolomite surface.

Radial distribution function (RDF) can describe the probability of finding gas molecules at distance r from the oil molecule, which was calculated by:

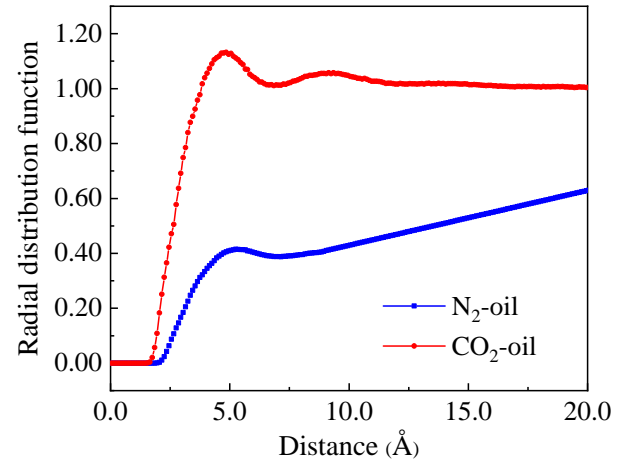


Fig. 6. Radial distribution function for the molecular mass centers of CO₂-C₈H₁₈ and N₂-C₈H₁₈.

$$g(r) = \frac{\rho(r)}{\rho_0} \quad (6)$$

where $\rho(r)$ represents the local density and ρ_0 is the bulk density.

Fig. 6 shows the RDFs between the CO₂ or N₂ and oil molecules after 0.5 ns of CO₂ flooding and 1.5 ns of N₂ flooding. It can be found that the first peak of RDF between CO₂ and oil molecules is located at 4.8 Å (line red), whereas the first peak of RDF between N₂ and oil molecules is lower at 5.3 Å (line blue). Hence, the interaction between CO₂ and oil molecules is stronger than that for N₂, which once again proves that CO₂ dissolves more easily in the oil phase.

Overall, the homogeneous conceptual slit model of dolomite on oil recovery was simulated at the nanoscale, which revealed the oil distribution and displacement process by density. We believe that these findings improve the understanding of CO₂-EOR and N₂-EOR process and benefit practical oil exploitation activities. However, our conceptual model of homogenization has limitations, it does not consider pore shape, roughness and matrix type, and the models are too

small, causing the simulation results to deviate from the real results. Further studies should be conducted at the macroscale simulations, whose scale is closer to the practical scale of underground oil reservoirs.

4. Conclusions

In the present study, the recovery of oil molecules from dolomite slit pore by CO₂ and N₂ flooding was investigated using molecular dynamics simulations, and the results showed that CO₂ and N₂ play different roles in the flooding process. CO₂ molecules have good dissolution and diffusion properties for replacing oil. The interaction energy between dolomite and CO₂ is stronger than that between dolomite and C₈H₁₈, thereby CO₂ can easily dislodge the oil adsorbed on the dolomite surface. For our dolomite slit pore model, at a pressure differential of 10 MPa and temperature of 333 K, CO₂ can dissolve and completely displace oil molecules, and the oil displacement efficiency can reach 100% after 1 ns of flooding. On the other hand, N₂ molecules cannot completely displace oil molecules adsorbed on dolomite surface due to the lower interaction energy between dolomite and N₂, and the oil displacement efficiency is 87.3% after 4 ns of flooding.

Acknowledgement

We would like to express our appreciation of the financial support by the National Natural Science Foundation of China (No. 51974342), and the Major Science and Technology Project of CNPC (2019E-2602).

Conflict of interest

The authors declare no competing interest.

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